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**ACRYLIC COPOLYMER COMPOSITION, METHOD FOR
PREPARING ACRYLIC COPOLYMER, AND VINYL CHLORIDE
RESIN COMPOSITION CONTAINING THE ACRYLIC COPOLYMER**

5 **Technical Field**

The present invention relates to an acrylic copolymer composition, a method for preparing an acrylic copolymer, and a vinyl chloride resin composition containing the acrylic copolymer. More particularly, the present
10 invention relates to an acrylic copolymer which improves the foamability of a vinyl chloride resin such as polyvinyl chloride (PVC) when used as an additive for the vinyl chloride resin and further improves the impact strength of the vinyl chloride resin when used in combination with an
15 impact modifier, and a vinyl chloride resin composition containing the same.

Background Art

Vinyl chloride resins are polymers containing 50% or
20 more of vinyl chloride. Since the vinyl chloride resins are inexpensive, are easy in hardness adjustment, and can be applied in most processing machines, they have various application fields. In addition, the vinyl chloride resins can be processed into formed products with good physical

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and chemical properties, and thus, are widely used in various fields.

However, the vinyl chloride resins have many disadvantages in impact strength, processability, thermal
5 stability, and heat deflection temperature. In this respect, additives for solving these disadvantages have been developed and used. Examples of additives for the vinyl chloride resins include impact modifiers, processing aids, stabilizers, and fillers, and are selectively used
10 according to their purposes.

Recently, there has been an increasing interest in a foam-forming process to decrease the mass of vinyl chloride resins and costs of formed products. However, foam-forming of only vinyl chloride resins cannot provide a sufficient
15 elongation and melt strength, which causes poor appearance of formed products and low expansion ratio due to large and non-uniform foamed cells. To solve these problems, addition of a mixture of a processing aid containing methyl methacrylate as a main component and a blowing agent to a
20 vinyl chloride resin is generally used.

U.S. Patent No. 6,140,417 discloses a vinyl chloride resin composition including a vinyl chloride resin and a processing aid for imparting improved processability and foamability to the vinyl chloride resin. The processing

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aid is prepared by three-stage polymerization of a compound selected from methyl methacrylate, alkyl acrylate, and alkyl methacrylate, and a copolymerizable vinyl monomer. The three-stage polymerization includes a first stage
5 polymerization for a low glass transition temperature (T_g), a second stage polymerization for a higher T_g than the first stage polymerization, and a third stage polymerization for a lower T_g than the second stage polymerization. U.S. Patent No. 6,221,966 discloses a
10 vinyl chloride resin composition including a vinyl chloride resin and a processing aid prepared by two-stage polymerization to impart improved processability, transparency, and foamability to the vinyl chloride resin. The processing aid has a small particle size, its inner
15 layer contains a small amount of methyl methacrylate for low T_g , and its outer layer contains a large amount of methyl methacrylate for high T_g . However, these vinyl chloride resin compositions are insufficient in terms of enhancement of processability and uniformity of foamed
20 cells.

U.S. Patent No. 6,391,976 discloses a vinyl chloride resin composition including a small quantity of a processing aid composed of methyl methacrylate and alkyl methacrylate of 3-5 carbon atoms. However, processability

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and foamability are insufficient.

In addition, there have been studies about combination of functions of several additives used to overcome many disadvantages of vinyl chloride resins, i.e., multi-purpose additives. Recently, in particular, studies about additives having combined characteristics of an impact modifier and a processing aid have been done. By way of example, European Patent No. EP 1,111,001 discloses a method for improving the impact strength of a vinyl chloride resin by adding powder particles composed of impact modifier particles and processing aid particles to the vinyl chloride resin, in which the powder particles are prepared by mixing an impact modifier and a processing aid in a latex phase, followed by coagulation and drying. However, this method is restrictive since latex mixing is required. Furthermore, this method is silent about information about formation of foamed products, and thus, a sufficient impact strength is not ensured.

Disclosure of Invention

In view of these problems, the present invention provides an acrylic copolymer composition which improves the foamability of a vinyl chloride resin when used as an additive for the vinyl chloride resin and further improves

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the impact strength of the vinyl chloride resin when used in combination with an impact modifier.

The present invention also provides a vinyl chloride resin composition containing an acrylic copolymer prepared
5 from the acrylic copolymer composition, which is excellent in foamability.

The present invention also provides a vinyl chloride resin composition containing an acrylic copolymer prepared from the acrylic copolymer composition and an impact
10 modifier, which is excellent in impact strength.

According to an aspect of the present invention, there is provided an acrylic copolymer composition including: (A) 5-15 wt% of a crosslinking agent and an alkyl acrylate monomer constituting an alkyl acrylate
15 crosslinked polymer; (B) 55-90 wt% of methyl methacrylate; and (C) 5-40 wt% of at least one monomer selected from the group consisting of an alkyl acrylate compound and an alkyl methacrylate compound.

The degree of swelling of the alkyl acrylate
20 crosslinked polymer may be in a range of 3 to 10.

The alkyl acrylate monomer constituting the alkyl acrylate crosslinked polymer may be an alkyl acrylate compound and the alkyl acrylate crosslinked polymer may be prepared from the crosslinking agent and the alkyl acrylate

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compound.

The crosslinking agent may be selected from the group consisting of allyl methacrylate, trimethylolpropane, triacrylate, and divinylbenzene.

- 5 The alkyl acrylate compound constituting the alkyl acrylate crosslinked polymer may have a straight, branched, or cyclic alkyl group of 1-18 carbon atoms.

 The alkyl acrylate compound constituting the alkyl acrylate crosslinked polymer may be one or more selected
10 from the group consisting of methyl acrylate, ethyl acrylate, n-butyl acrylate, lauryl acrylate, stearyl acrylate, 2-ethylhexyl acrylate, and cyclohexyl acrylate.

 The alkyl acrylate compound of the monomer (C) may have a straight, branched, or cyclic alkyl group of 1-18
15 carbon atoms and the alkyl methacrylate compound of the monomer (C) may have a straight or cyclic alkyl group of 2-18 carbon atoms.

 The alkyl acrylate compound of the monomer (C) may be one or more selected from the group consisting of methyl
20 acrylate, ethyl acrylate, n-butyl acrylate, lauryl acrylate, stearyl acrylate, 2-ethylhexyl acrylate, and cyclohexyl acrylate. The alkyl methacrylate compound of the monomer (C) may be one or more selected from the group consisting of n-butyl methacrylate, lauryl methacrylate, stearyl

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methacrylate, tridecyl methacrylate, i-butyl methacrylate, t-butyl methacrylate, 2-ethylhexyl methacrylate, and cyclohexyl methacrylate.

The acrylic copolymer may have a weight average
5 molecular weight of 1,000,000 to 12,000,000.

According to another aspect of the present invention, there is provided a method for preparing an acrylic copolymer, which includes emulsion polymerization, suspension polymerization, or solution polymerization of 5-
10 15 wt% of a crosslinking agent and an alkyl acrylate monomer constituting an alkyl acrylate crosslinked polymer having the degree of swelling of 3 to 10; 55-90 wt% of methyl methacrylate; and 5-40 wt% of at least one monomer selected from the group consisting of an alkyl acrylate
15 compound and an alkyl methacrylate compound.

The emulsion polymerization preparing an acrylic copolymer may include (a) (i) mixing 5-15 wt% of the crosslinking agent and the alkyl acrylate monomer to prepare an emulsion containing the alkyl acrylate
20 crosslinked polymer having the degree of swelling of 3 to 10 and adding 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the at least one monomer selected from the group consisting of the alkyl acrylate compound with an alkyl group of 1-18 carbon atoms and the alkyl methacrylate

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compound with an alkyl group of 2-18 carbon atoms, an emulsifier, a polymerization initiator, and a redox catalyst, to the emulsion containing the alkyl acrylate crosslinked polymer or (ii) mixing 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the at least one monomer selected from the group consisting of the alkyl acrylate compound and the alkyl methacrylate compound, the emulsifier, the polymerization initiator, and the redox catalyst, and adding 5-15 wt% of the crosslinking agent and the alkyl acrylate monomer to the mixture; and (b) further adding 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the at least one monomer selected from the group consisting of the alkyl acrylate compound and the alkyl methacrylate compound, the emulsifier, the polymerization initiator, and the redox catalyst, to the resultant mixture of step (a).

According to another aspect of the present invention, there is provided a vinyl chloride resin composition including a vinyl chloride resin and 0.1-20 parts by weight of an acrylic copolymer prepared according to the method, based on 100 parts by weight of the vinyl chloride resin.

According to yet another aspect of the present invention, there is provided a vinyl chloride resin composition including a vinyl chloride resin and 1-30 parts

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by weight of a mixture comprising 5-30 wt% of an acrylic copolymer prepared according to the method and 70-95 wt% of an impact modifier, based on the 100 parts by weight of the vinyl chloride resin.

5 The impact modifier may be selected from the group consisting of acrylonitrile-butadiene-styrene (ABS), methyl methacrylate-butadiene-styrene (MBS), and acrylic compounds.

Hereinafter, the present invention will be described in more detail.

10 An acrylic copolymer prepared from an acrylic copolymer composition including a specific crosslinked polymer and a non-crosslinked polymer in a predetermined ratio according to the present invention improves the foamability of a vinyl chloride resin when added to the
15 vinyl chloride resin. Further, when a mixture of the acrylic copolymer and an impact modifier is used as an additive for the vinyl chloride resin, the vinyl chloride resin can have a higher impact strength, as compared to when the impact modifier is used alone.

20 That is, the acrylic copolymer composition of the present invention includes 5-15 wt% of a crosslinking agent and an alkyl acrylate monomer constituting an alkyl acrylate crosslinked polymer; and 55-90 wt% of methyl methacrylate and 5-40 wt% of at least one selected from the

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group consisting of an alkyl acrylate compound and an alkyl methacrylate compound constituting a non-crosslinked copolymer.

Preferably, the alkyl acrylate crosslinked polymer
5 has the degree of swelling from 3 to 10 to lower its glass transition temperature. The alkyl acrylate crosslinked polymer serves to increase the degree of swelling of the acrylic copolymer of the present invention, thereby enhancing die swell characteristics, and is prepared from a
10 crosslinking agent and an alkyl acrylate compound. If the degree of swelling is less than 3, good die swell characteristics may not be obtained. On the other hand, if it exceeds 10, processability suitable for a vinyl chloride resin may not be ensured, which makes it difficult to
15 produce a good foamed product.

Preferably, the crosslinking agent and the alkyl acrylate monomer constituting the alkyl acrylate crosslinked polymer are used in an amount of 5 to 15 wt%. If the content of the crosslinking agent and the alkyl
20 acrylate monomer is less than 5 wt%, a formed product may have an insufficient expansion ratio. On the other hand, if it exceeds 15 wt%, fine and uniform foamed cells may not be obtained.

Preferably, the crosslinking agent is allyl

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methacrylate, trimethylolpropane, triacrylate,
divinylbenzene, or the like.

Preferably, the alkyl acrylate compound constituting
the alkyl acrylate crosslinked polymer has a straight,
5 branched, or cyclic alkyl group of 1-18 carbon atoms. More
preferably, the alkyl acrylate compound is methyl acrylate,
ethyl acrylate, n-butyl acrylate, lauryl acrylate, stearyl
acrylate, 2-ethylhexyl acrylate, or cyclohexyl acrylate.

Preferably, the methyl methacrylate constituting the
10 non-crosslinked polymer is used in an amount of 55-90 wt%,
based on the total weight of the acrylic copolymer
composition. If the content of the methyl methacrylate is
less than 55 wt%, compatibility with a vinyl chloride resin
may be lowered, thereby deteriorating processability. On
15 the other hand, if it exceeds 90 wt%, dispersibility in a
vinyl chloride resin composition may be lowered, thereby
producing fish-eyes. More preferably, the methyl
methacrylate is used in an amount of 70 to 80 wt%.

Preferably, the alkyl acrylate compound constituting
20 the non-crosslinked copolymer has a straight, branched, or
cyclic alkyl group of 1-18 carbon atoms and the alkyl
methacrylate compound constituting the non-crosslinked
copolymer has a straight or cyclic alkyl group of 2-18
carbon atoms. More preferably, the alkyl acrylate compound

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is methyl acrylate, ethyl acrylate, n-butyl acrylate,
lauryl acrylate, stearyl acrylate, 2-ethylhexyl acrylate,
or cyclohexyl acrylate, and the alkyl methacrylate compound
is n-butyl methacrylate, lauryl methacrylate, stearyl
5 methacrylate, tridecyl methacrylate, i-butyl methacrylate,
t-butyl methacrylate, 2-ethylhexyl methacrylate, or
cyclohexyl methacrylate.

Preferably, the weight average molecular weight of an
acrylic copolymer, except a crosslinked polymer component,
10 prepared from the above-described composition is in a range
of 1,000,000 to 12,000,000.

A method for preparing an acrylic copolymer is not
limited by polymerization methods. Preferably, emulsion
polymerization, suspension polymerization or solution
15 polymerization are used and the emulsion polymerization is
more preferable.

That is, a method for preparing an acrylic copolymer
by an emulsion polymerization according to the present
invention may include (a) (i) mixing 5-15 wt% of a
20 crosslinking agent and an alkyl acrylate monomer to prepare
an emulsion containing an alkyl acrylate crosslinked
polymer having the degree of swelling of 3 to 10 and adding
27.5-45 wt% of methyl methacrylate, 2.5-20 wt% of at least
one monomer selected from the group consisting of an alkyl

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acrylate compound with an alkyl group of 1-18 carbon atoms and an alkyl methacrylate compound with an alkyl group of 2-18 carbon atoms, an emulsifier, a polymerization initiator, and a redox catalyst, to the emulsion containing

5 the alkyl acrylate crosslinked polymer or (ii) mixing 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the at least one monomer selected from the group consisting of the alkyl acrylate compound with an alkyl group of 1-18 carbon atoms and the alkyl methacrylate compound with an alkyl

10 group of 2-18 carbon atoms, the emulsifier, the polymerization initiator, and the redox catalyst, and adding 5-15 wt% of the crosslinking agent and the alkyl acrylate monomer to the mixture; and (b) further adding 27.5-45 wt% of the methyl methacrylate, 2.5-20 wt% of the

15 at least one monomer selected from the group consisting of the alkyl acrylate compound with an alkyl group of 1-18 carbon atoms and the alkyl methacrylate compound with an alkyl group of 2-18 carbon atoms, the emulsifier, the polymerization initiator, and the redox catalyst, to the

20 resultant mixture of step (a).

Preferably, the emulsifier is used in an amount of 0.5 to 5 wt%, based on the total weight of all components used in the preparation of the acrylic copolymer. There are no particular limitations on the type of the emulsifier

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that can be used herein. However, it is preferable to use, as the emulsifier, an anionic emulsifier such as aliphatic ester, alkyl benzene sulfonate, alkyl phosphate, and dialkyl sulfosuccinate, and a non-ionic emulsifier such as
5 polyoxyethylene alkyl ether and alkylamine ester, alone or in combination.

Preferably, the crosslinking agent is used in an amount of 0.01 to 0.3 wt%, based on the total weight of all components used in the preparation of the acrylic copolymer.
10 The crosslinking agent may be allyl methacrylate, trimethylolpropane, triacrylate, or divinylbenzene. An acrylate compound is more preferable.

Preferably, the polymerization initiator is used in an amount of 0.0005 to 0.005 wt%, based on the total weight
15 of all components used in the preparation of the acrylic copolymer. The polymerization initiator may be a water-soluble initiator such as potassium persulfate, ammonium persulfate, and sodium persulfate, an oil-soluble initiator such as t-butyl hydroperoxide, cumene hydroperoxide,
20 benzoyl peroxide, and lauryl peroxide, or a redox initiator.

Preferably, the redox catalyst is used in an amount of 0.01 to 0.1 wt%, based on the total weight of all components used in the preparation of the acrylic copolymer. The redox catalyst may be sodium formaldehydesulfoxylate,

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disodium ethylenediaminetetraacetate, sodium formaldehyde sulfoxylate, ferrous sulfate, sodium ethylenediaminetetraacetate, or cupric sulfate.

A latex acrylic copolymer prepared by the emulsion
5 polymerization is converted to a powdery acrylic copolymer by coagulation, dehydration, and drying.

The acrylic copolymer prepared as described above can be contained in a vinyl chloride resin composition to impart good foamability to a vinyl chloride resin.

10 Therefore, the present invention also provides a vinyl chloride resin composition including a vinyl chloride resin and 0.1 to 20 parts by weight of the acrylic copolymer, based on 100 parts by weight of the vinyl chloride resin. A use of the acrylic copolymer within the above content
15 range can enhance a melt strength and a die swell property which are important factors for extrusion-foaming of the vinyl chloride resin, resulting in a foamed product which is excellent in foam density, expansion ratio, uniformity of foamed cells, and the like.

20 The present invention also provides a vinyl chloride resin composition including a vinyl chloride resin and 1-30 parts by weight of a mixture comprising 5-30 wt% of the acrylic copolymer and 70-95 wt% of an impact modifier, based on 100 parts by weight of the vinyl chloride resin.

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The combination of the acrylic copolymer of the present invention and the impact modifier can provide a higher impact strength, as compared to when the impact modifier is used alone, which makes it possible to produce a formed
5 product with a sufficient impact strength.

Preferably, the impact modifier is acrylonitrile-butadiene-styrene (ABS), methyl methacrylate-butadiene-styrene (MBS), or an acrylic modifier. The acrylic modifier is more preferable in terms of weatherability of a
10 formed product.

Hereinafter, the present invention will be described more specifically by Examples but the present invention is not limited to or by them.

15 **Modes for Carrying Out the Invention**

Examples 1-10 and Comparative Examples 1-7:

Preparation of acrylic copolymers

[Example 1]

(1) Preparation of acrylic copolymer

20 420 g of ion exchange water, 10 g of a 8% potassium salt solution of fatty acid, 59.5 g of butyl acrylate, and 0.5 g of allyl methacrylate were placed in a 3l four-necked flask reactor equipped with a stirrer, a thermocouple, a nitrogen inlet, and a reflux condenser, to prepare an

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emulsion. Then, the reactor was maintained at an internal temperature of 62°C under a nitrogen atmosphere and 0.45 g of t-butyl hydroperoxide (10% diluted solution) and 12 g of an activation solution were added to the reactor to perform
5 a primary batch reaction. As the activation solution, there was used a mixture of 0.017 g of disodium ethylenediaminetetraacetate (EDTA), 0.04 g of sodium formaldehyde sulfoxylate (SFS), 0.001 g of ferrous sulfate, and 1.406 g of ion exchange water.

10 After the primary batch reaction was terminated, the reactor was stirred at the same temperature for one hour and then maintained at an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared
15 by mixing 229.5 g of methyl methacrylate and 40.5 g of butyl acrylate in a ratio of 85:15 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere and 0.3 g of t-butyl hydroperoxide (10%
20 diluted solution) and 6.7 g of the same activation solution as used for the primary batch reaction were added to the reactor to perform a secondary batch reaction.

After the secondary batch reaction was terminated, the reactor was further stirred for 1.5 hours and then

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maintained at an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 229.5 g of methyl methacrylate and 40.5 g of butyl acrylate in a ratio of 85:15 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as used for the primary batch reaction were added to the reactor to perform a tertiary batch reaction.

After the tertiary batch reaction was terminated, the reactor was further stirred for one hour to give a latex acrylic copolymer. The latex acrylic copolymer was subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic copolymer.

Main components used in each reaction process for the preparation of the acrylic copolymer of Example 1 and acrylic copolymers of Examples 2-10 and Comparative Examples 1-7 as will be described later are summarized in Table 1 below.

(2) Measurement of degree of swelling and weight average molecular weight of acrylic copolymer

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0.3 g of the powdery acrylic copolymer as prepared in
Section (1) was dissolved in 100 ml of tetrahydrofuran
(THF) for 50 hours and centrifuged at 16,000 rpm for 2
hours. After the centrifugation, a swelled gel and a sol
5 were separated to measure the weight of the swelled gel.
The swelled gel was then dried to measure the weight of the
dried gel. The degree of swelling of the powdery acrylic
copolymer was calculated according to the following
Equation 1 and the result is presented in Table 2 below:

10 [Equation 1]

$$\text{Degree of swelling} = \frac{\text{weight of swelled gel}}{\text{weight of dried gel}}$$

Furthermore, the weight average molecular weight of
15 the sol of the acrylic copolymer was measured using gel
permeation chromatography (GPC) and the result is presented
in Table 2 below. The weight average molecular weight of
the acrylic copolymer except the crosslinked polymer
component was 4,300,000.

20

[Example 2]

An acrylic copolymer was prepared in the same manner
as in Example 1 except that ethyl acrylate was used in the
primary batch reaction, instead of the butyl acrylate. The

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degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

5 [Example 3]

 An acrylic copolymer was prepared in the same manner as in Example 1 except that 59.5 g of a monomer mixture prepared by mixing ethyl acrylate and butyl acrylate in a ratio of 1:1 was used in the primary batch reaction,
10 instead of 59.5 g of the butyl acrylate. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

15 [Example 4]

 An acrylic copolymer was prepared in the same manner as in Example 1 except that a monomer mixture prepared by mixing 216 g of methyl methacrylate and 54 g of butyl acrylate in a ratio of 80:20 was used in the secondary and
20 tertiary batch reactions. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

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[Example 5]

532 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 216 g of methyl methacrylate and 54 g of butyl acrylate in a ratio of 80:20 were placed in a 3l four-necked flask reactor equipped with a stirrer, a thermocouple, a nitrogen inlet, and a reflux condenser, to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a primary batch reaction.

After the primary batch reaction was terminated, the reactor was stirred at the same temperature for one hour. Then, 50 g of ion exchange water, 10 g of a 8% potassium salt solution of fatty acid, 59.5 g of butyl acrylate, and 0.5 g of allyl methacrylate were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 62°C under a nitrogen atmosphere and 0.45 g of t-butyl hydroperoxide (10% diluted solution) and 12 g of the same activation solution as in Example 1 were added to the reactor to perform a secondary batch reaction.

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After the secondary batch reaction was terminated, the reactor was further stirred for 1.5 hours and then maintained at an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 216 g of methyl methacrylate and 54 g of butyl acrylate in a ratio of 80:20 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a tertiary batch reaction.

After the tertiary batch reaction was terminated, the reactor was further stirred for one hour to give a latex acrylic copolymer. The latex acrylic copolymer was subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic copolymer. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

[Example 6]

532 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 216 g of methyl methacrylate and 54 g of butyl

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acrylate in a ratio of 80:20 were added to a 3l four-necked flask reactor equipped with a stirrer, a thermocouple, a nitrogen inlet, and a reflux condenser, to prepare an emulsion. Then, the reactor was maintained at an internal
5 temperature of 40°C under a nitrogen atmosphere, and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a primary batch reaction.

After the primary batch reaction was terminated, the
10 reactor was further stirred for 1.5 hours and maintained at an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 216 g of methyl methacrylate and 54 g of butyl acrylate in a
15 ratio of 80:20 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere, and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added
20 to the reactor to perform a secondary batch reaction.

After the secondary batch reaction was terminated, the reactor was further stirred for 1.5 hours. Then, 50 g of ion exchange water, 10 g of a 8% potassium salt solution of fatty acid, 59.5 g of butyl acrylate, and 0.5 g of allyl

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methacrylate were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 62°C under a nitrogen atmosphere and 0.45 g of t-butyl hydroperoxide (10% diluted solution) and 12 g of
5 the same activation solution as in Example 1 were added to the reactor to perform a tertiary batch reaction.

After the tertiary batch reaction was terminated, the reactor was further stirred for one hour to give a latex acrylic copolymer. The latex acrylic copolymer was
10 subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic copolymer. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

15

[Example 7]

An acrylic copolymer was prepared in the same manner as in Example 4 except that ethyl acrylate was used in the primary batch reaction, instead of the butyl acrylate. The
20 degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

[Example 8]

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An acrylic copolymer was prepared in the same manner as in Example 4 except that 59.5 g of a monomer mixture prepared by mixing ethyl acrylate and butyl acrylate in a ratio of 1:1 was used in the primary batch reaction,
5 instead of 59.5 g of the butyl acrylate. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

10 [Example 9]

An acrylic copolymer was prepared in the same manner as in Example 4 except that 0.1 g of the t-butyl hydroperoxide (10% diluted solution) and 3.4 g of the activation solution were used in the secondary and tertiary
15 batch reactions. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

[Example 10]

20 An acrylic copolymer was prepared in the same manner as in Example 4 except that in the secondary and tertiary batch reactions, the internal temperature of the reactor was maintained at 35°C and 0.06 g of the t-butyl hydroperoxide (10% diluted solution) and 2.3 g of the

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activation solution were used. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

5

[Comparative Example 1]

An acrylic copolymer was prepared in the same manner as in Example 1 except that allyl methacrylate as a crosslinking agent was not used in the primary batch
10 reaction. The weight average molecular weight of the acrylic copolymer was measured by GPC using THF as a mobile phase and the result is presented in Table 2 below.

The weight average molecular weights of the acrylic copolymer of Comparative Example 1 and acrylic copolymers
15 of Comparative Examples 2 and 7 as will be described later were measured by GPC using THF as a mobile phase.

[Comparative Example 2]

An acrylic copolymer was prepared in the same manner
20 as in Example 5 except that allyl methacrylate as a crosslinking agent was not used in the secondary batch reaction. The weight average molecular weight of the acrylic copolymer was measured by GPC using THF as a mobile phase and the result is presented in Table 2 below.

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[Comparative Example 3]

An acrylic copolymer was prepared in the same manner as in Example 1 except that 58.5 g of butyl acrylate and
5 1.5 g of allyl methacrylate were used in the primary batch reaction. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

10 [Comparative Example 4]

An acrylic copolymer was prepared in the same manner as in Example 1 except that 59.9 g of butyl acrylate and 0.1 g of allyl methacrylate were used in the primary batch reaction. The degree of swelling and weight average
15 molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

[Comparative Example 5]

An acrylic copolymer was prepared in the same manner
20 as in Example 4 except that 26.78 g of butyl acrylate and 0.22 g of allyl methacrylate were used in the primary batch reaction and a monomer mixture prepared by mixing 229.2 g of methyl methacrylate and 57.3 g of butyl acrylate in a ratio of 80:20 was used in the secondary and tertiary batch

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reactions. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

5 [Comparative Example 6]

An acrylic copolymer was prepared in the same manner as in Example 4 except that 92.23 g of butyl acrylate and 0.77 g of allyl methacrylate were used in the primary batch reaction and a monomer mixture prepared by mixing 202.8 g
10 of methyl methacrylate and 50.7 g of butyl acrylate in a ratio of 80:20 was used in the secondary and tertiary batch reactions. The degree of swelling and weight average molecular weight of the acrylic copolymer were measured and the results are presented in Table 2 below.

15

[Comparative Example 7]

420 g of ion exchange water, 10 g of a 8% potassium salt solution of fatty acid, 51 g of methyl methacrylate, and 9 g of butyl acrylate were placed in a 3ℓ four-necked
20 flask reactor equipped with a stirrer, a thermocouple, a nitrogen inlet, and a reflux condenser, to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 62°C under a nitrogen atmosphere and 0.45 g of t-butyl hydroperoxide (10% diluted solution) and 12 g of

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the same activation solution as in Example 1 were added to the reactor to perform a primary batch reaction.

After the primary batch reaction was terminated, the reactor was stirred at the same temperature for one hour
5 and then adjusted to an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution of fatty acid, and a monomer mixture prepared by mixing 229.5 g of methyl methacrylate and 40.5 g of butyl acrylate in a ratio of 85:15 were added to the reactor to
10 prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere, and 0.3 g of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a secondary batch
15 reaction.

After the secondary batch reaction was terminated, the reactor was further stirred for 1.5 hours and then adjusted to an internal temperature of 40°C. Then, 162 g of ion exchange water, 25 g of a 8% potassium salt solution
20 of fatty acid, and a monomer mixture prepared by mixing 229.5 g of methyl methacrylate and 40.5 g of butyl acrylate in a ratio of 85:15 were added to the reactor to prepare an emulsion. Then, the reactor was maintained at an internal temperature of 40°C under a nitrogen atmosphere, and 0.3 g

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of t-butyl hydroperoxide (10% diluted solution) and 6.7 g of the same activation solution as in Example 1 were added to the reactor to perform a tertiary batch reaction.

After the tertiary batch reaction was terminated, the
5 reactor was further stirred for one hour to give a latex acrylic copolymer. The latex acrylic copolymer was subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic copolymer. The weight average molecular weight of the powdery acrylic
10 copolymer was measured by GPC using THF as a mobile phase and the result is presented in Table 2 below.

Examples 11-20 and Comparative Examples 8-14:

Preparation of vinyl chloride resins with good foaming
15 property using acrylic copolymers

[Example 11]

(1) Preparation of vinyl chloride resin modified by
acrylic copolymer (with filler)

6.4 g of a composite stabilizer KD-105 (Dansuk
20 Industrial Co., Ltd.) prepared by uniformly mixing a thermal stabilizer and a lubricant, which is used as both a thermal stabilizer and a foam stabilizer, and 14 g of a filler (CaCO_3) were added to 100 g of a vinyl chloride resin (LS080, LG Chemical, Co., Ltd.). Then, 5 g of the

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acrylic copolymer prepared in Example 1 and 0.8 g of azodicarbonamide were added and mixed by a Henschel mixer with heating to 115°C to prepare a vinyl chloride resin modified with the acrylic copolymer.

5

(2) Measurement of melt time of vinyl chloride resin

64 g of the vinyl chloride resin prepared in Section (1) was mixed at 180°C and 40 rpm in a Brabender. Then, a melt time defined as a time required from minimum load to
10 maximum load was measured and is presented in Table 2 below.

(3) Evaluation of foaming property of vinyl chloride resin

The vinyl chloride resin prepared in Section (1) was
15 extruded in the form of a rectangular rod of 5 mm (thickness) × 30 mm (width) using a 30 mm single spindle extruder equipped with a rectangular slit die at a cylinder temperature of 180°C and a screw speed of 30 rpm and then cut into length of 5 mm. The foam density of the foamed
20 products thus obtained was measured using a gravimeter and the result is presented in Table 2 below. As the foam density decreases, foaming property is good.

Meanwhile, based on an expansion ratio defined as the ratio (a/b) of the foam density (a) of a foamed product

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with no acrylic copolymer to the foam density (b) of a foamed product with acrylic copolymer, the expansion ratio of the foamed products of this Example was calculated and the result is presented in Table 2 below.

5 In addition, the sections of the foamed products were observed with an optical microscope. Scoring criteria were as follows: 5 = uniform foamed cells, 3 = slightly non-uniform foamed cells, and 1 = non-uniform foamed cells. The results are presented in Table 2 below.

10

(4) Preparation of vinyl chloride resin modified by acrylic copolymer (with no filler)

A vinyl chloride resin was prepared in the same manner as in Section (1) except that no fillers were used.

15

(5) Measurement of fish-eyes in vinyl chloride resin

The vinyl chloride resin prepared in Section (4) was extruded in the form of 0.2 mm thickness film using a 20 mm single spindle extruder equipped with a T-die at a cylinder
20 temperature of 180°C and screw speed of 30 rpm and then the number of fish-eyes present in a predetermined surface region of the film was counted with a naked eye. Scoring criteria were as follows: 5 = few fish-eyes, 3 = a few fish-eyes, and 1 = many fish-eyes. The evaluation result

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is presented in Table 2 below.

[Example 12]

A vinyl chloride resin was prepared in the same
5 manner as in Example 11 using the acrylic copolymer of
Example 2. The melt time, foaming property, and the number
of fish-eyes of the vinyl chloride resin were evaluated and
the evaluation results are presented in Table 2 below.

10 [Example 13]

A vinyl chloride resin was prepared in the same
manner as in Example 11 using the acrylic copolymer of
Example 3. The melt time, foaming property, and the number
of fish-eyes of the vinyl chloride resin were evaluated and
15 the evaluation results are presented in Table 2 below.

[Example 14]

A vinyl chloride resin was prepared in the same
manner as in Example 11 using the acrylic copolymer of
20 Example 4. The melt time, foaming property, and the number
of fish-eyes of the vinyl chloride resin were evaluated and
the evaluation results are presented in Table 2 below.

[Example 15]

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A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 5. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and
5 the evaluation results are presented in Table 2 below.

[Example 16]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of
10 Example 6. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

[Example 17]

15 A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 7. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

20

[Example 18]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 8. The melt time, foaming property, and the number

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of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

[Example 19]

5 A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 9. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

10

[Example 20]

A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Example 10. The melt time, foaming property, and the
15 number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in Table 2 below.

[Comparative Example 8]

20 A vinyl chloride resin was prepared in the same manner as in Example 11 using the acrylic copolymer of Comparative Example 1. The melt time, foaming property, and the number of fish-eyes of the vinyl chloride resin were evaluated and the evaluation results are presented in

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Table 2 below.

[Comparative Example 9]

A vinyl chloride resin was prepared in the same
5 manner as in Example 11 using the acrylic copolymer of
Comparative Example 2. The melt time, foaming property,
and the number of fish-eyes of the vinyl chloride resin
were evaluated and the evaluation results are presented in
Table 2 below.

10

[Comparative Example 10]

A vinyl chloride resin was prepared in the same
manner as in Example 11 using the acrylic copolymer of
Comparative Example 3. The melt time, foaming property,
15 and the number of fish-eyes of the vinyl chloride resin
were evaluated and the evaluation results are presented in
Table 2 below.

[Comparative Example 11]

20 A vinyl chloride resin was prepared in the same
manner as in Example 11 using the acrylic copolymer of
Comparative Example 4. The melt time, foaming property,
and the number of fish-eyes of the vinyl chloride resin
were evaluated and the evaluation results are presented in

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Table 2 below.

[Comparative Example 12]

A vinyl chloride resin was prepared in the same
5 manner as in Example 11 using the acrylic copolymer of
Comparative Example 5. The melt time, foaming property,
and the number of fish-eyes of the vinyl chloride resin
were evaluated and the evaluation results are presented in
Table 2 below.

10

[Comparative Example 13]

A vinyl chloride resin was prepared in the same
manner as in Example 11 using the acrylic copolymer of
Comparative Example 6. The melt time, foaming property,
15 and the number of fish-eyes of the vinyl chloride resin
were evaluated and the evaluation results are presented in
Table 2 below.

[Comparative Example 14]

20 A vinyl chloride resin was prepared in the same
manner as in Example 11 using the acrylic copolymer of
Comparative Example 7. The melt time, foaming property,
and the number of fish-eyes of the vinyl chloride resin
were evaluated and the evaluation results are presented in

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Table 2 below.

5

Table 1

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Section	Main components (g) of each reaction		
	Primary reaction	Secondary reaction	Tertiary reaction
Exam. 1	Butyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Exam. 2	Ethyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Exam. 3	1:1 mixture of butyl acrylate and ethyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Exam. 4	Butyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam. 5	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Butyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam. 6	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Butyl acrylate (59.5) allyl methacrylate (0.5)
Exam. 7	Ethyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam. 8	1:1 mixture of butyl acrylate and ethyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam. 9	Butyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Exam.10	Butyl acrylate (59.5) allyl methacrylate (0.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Comp. 1	Butyl acrylate (59.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Comp. 2	Methyl methacrylate (216.0) Butyl acrylate (54.0)	Butyl acrylate (59.5)	Methyl methacrylate (216.0) Butyl acrylate (54.0)
Comp. 3	Butyl acrylate (58.5) allyl methacrylate (1.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Comp. 4	Butyl acrylate (59.9) allyl methacrylate (0.1)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)
Comp. 5	Butyl acrylate (26.78) allyl methacrylate (0.22)	Methyl methacrylate (229.2) Butyl acrylate (57.3)	Methyl methacrylate (229.2) Butyl acrylate (57.3)
Comp. 6	Butyl acrylate (92.23) allyl methacrylate (0.77)	Methyl methacrylate (202.8) Butyl acrylate (50.7)	Methyl methacrylate (202.8) Butyl acrylate (50.7)
Comp. 7	Methyl methacrylate (51.0) Butyl acrylate (9.0)	Methyl methacrylate (229.5) Butyl acrylate (40.5)	Methyl methacrylate (229.5) Butyl acrylate (40.5)

Exam.: Example, Comp.: Comparative Example

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Table 2

Section	Degree of swelling	WAMW ($\times 10,000$)	Section	Melt time (s)	Fish eye	Foaming property		
						Foam density (g/cm ³)	Expansion ratio	Uniformity of foamed cells
Exam. 1	6.1	430	Exam. 11	93	4.0	0.72	1.65	4.5
Exam. 2	6.6	410	Exam. 12	89	4.0	0.73	1.63	4.0
Exam. 3	6.3	410	Exam. 13	92	4.0	0.73	1.63	4.5
Exam. 4	6.2	420	Exam. 14	90	5.0	0.71	1.68	4.5
Exam. 5	5.9	410	Exam. 15	88	5.0	0.72	1.65	4.0
Exam. 6	5.6	410	Exam. 16	88	4.0	0.73	1.63	4.0
Exam. 7	6.1	410	Exam. 17	88	5.0	0.73	1.63	4.0
Exam. 8	6.5	420	Exam. 18	90	5.0	0.74	1.61	4.5
Exam. 9	6.0	650	Exam. 19	93	5.0	0.68	1.75	5.0
Exam. 10	5.8	910	Exam. 20	95	5.0	0.67	1.78	5.0
Comp. 1	-	400	Comp. 8	90	5.0	0.79	1.51	3.0
Comp. 2	-	410	Comp. 9	88	5.0	0.77	1.55	3.0
Comp. 3	2.3	420	Comp. 10	89	4.0	0.79	1.51	3.0
Comp. 4	11.2	440	Comp. 11	85	4.0	0.72	1.65	3.0
Comp. 5	6.2	450	Comp. 12	87	5.0	0.79	1.51	3.5
Comp. 6	6.4	400	Comp. 13	92	4.0	0.73	1.63	3.0
Comp. 7	-	400	Comp. 14	98	4.0	0.82	1.45	4.0

Exam.: Example, Comp.: Comparative Example, WAMW: weight average

molecular weight

5

As shown in Table 2, the vinyl chloride resins of Examples 11-20 prepared using the acrylic copolymers of Examples 1-10 in which a crosslinked polymer was prepared from allyl methacrylate as a crosslinking agent and alkyl acrylate, exhibited superior foam density, expansion ratio,

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and uniformity of foamed cells, as compared to the vinyl chloride resins of Comparative Examples 8 and 9 prepared using the acrylic copolymers of Comparative Examples 1 and 2 in which no crosslinked polymers were prepared due to the
5 absence of a crosslinking agent such as allyl methacrylate.

Furthermore, the vinyl chloride resin of Comparative Example 10 prepared using the acrylic copolymer of Comparative Example 3 having the degree of swelling of 2.3
10 exhibited poor die swell property, thereby lowering an expansion ratio, as compared to the vinyl chloride resins of Examples 11-20 prepared using the acrylic copolymers of Examples 1-10 having the degree of swelling of 3 to 10. The vinyl chloride resin of Comparative Example 11 prepared
15 using the acrylic copolymer of Comparative Example 4 having the degree of swelling of 11.2 exhibited a high expansion ratio but poor processability, thereby lowering foaming properties.

The vinyl chloride resin of Comparative Example 12
20 prepared using the acrylic copolymer of Comparative Example 5, in which the content of alkyl acrylate and a crosslinking agent was 4.5 wt% per the total weight of all the monomers used in the preparation of the acrylic copolymer, exhibited a low expansion ratio, resulting in a

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poor foamed product. On the other hand, the vinyl chloride resin of Comparative Example 13 prepared using the acrylic copolymer of Comparative Example 6, in which the content of alkyl acrylate and a crosslinking agent was 15.5 wt% per
5 the total weight of all the monomers used in the preparation of the acrylic copolymer, produced non-uniform foamed cells.

The vinyl chloride resin of Comparative Example 14 prepared using the acrylic copolymer of Comparative Example
10 7, in which no crosslinked polymer was prepared due to the absence of a crosslinking agent such as allyl methacrylate, produced a foamed product with low expansion ratio.

The vinyl chloride resins of Examples 19 and 20 prepared using the acrylic copolymers of Examples 9 and 10
15 exhibited an increased melt strength due to the high molecular weight of the acrylic copolymers, resulting in uniform foamed cells.

From the above Examples and Comparative Examples, it can be seen that when an acrylic copolymer contains a
20 crosslinked polymer with a predetermined swelling degree and has a high molecular weight, foaming property is enhanced. This is because the vinyl chloride resins of Examples have good melt strength and die swell property, thereby ensuring a low foam density and uniform foamed

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cells, as compared to those of Comparative Examples.

Examples 21-26 and Comparative Examples 15-17:

Preparation of vinyl chloride resins with good impact

5 strength using acrylic copolymers

[Example 21]

(1) Preparation of acrylic impact modifier

415.8 g of ion exchange water was added to a reactor
10 which was then heated to 78°C with nitrogen washing. When
the ion exchange water reached 78°C, 43.56 g of butyl
acrylate, 0.72 g of 1,3-butanediol diacrylate, 0.72 g of
methacrylic acid, and 24.21 g of 8 % potassium salt
solution of fatty acid were at a time added to the reactor.
15 While the internal temperature of the reactor was
maintained at 78°C, a seed reaction was carried out by
addition of 12.6 g of 3% potassium persulfate solution to
prepare a rubber latex. The nitrogen washing was continued
until the seed reaction was terminated.

20 276.45 g of the rubber latex prepared by the seed
reaction and 9.37 g of 8% potassium salt solution of fatty
acid were sequentially added to a reactor which was then
heated to 78°C with nitrogen washing and stirred at 15°C to
obtain a pre-emulsion. Then, a mixture of 180.3 g of ion

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exchange water, 288.9 g of butyl acrylate, 0.35 g of 1,3-butanediol diacrylate, 0.75 g of allyl methacrylate, 34.67 g of 8% potassium salt solution of fatty acid, and 8.33 g of 3% potassium persulfate solution was added to the
5 reactor to perform a primary core reaction. The reactor was maintained at 78°C and the nitrogen washing was continued until the core reaction was terminated.

A mixture of 59.2 g of ion exchange water, 109.2 g of butyl acrylate, 0.15 g of 1,3-butanediol diacrylate, 0.65 g
10 of allyl methacrylate, 15.62 g of 8% potassium salt solution of fatty acid, and 6.67 g of 3% potassium persulfate solution was stirred to obtain a pre-emulsion. The pre-emulsion was added to the reactor containing a product of the primary core reaction using a pump for one
15 hour to perform a secondary core reaction and then incubated for one hour. The reactor was maintained at 78°C and nitrogen washing was continued until the secondary core reaction was terminated.

A mixture of 97.4 g of ion exchange water, 71.25 g of
20 methyl methacrylate, 3.75 g of ethyl acrylate, 2.8 g of acrylonitrile, 9.37 g of 8% potassium salt solution of fatty acid, and 6.33 g of 3% potassium persulfate solution was sufficiently stirred to obtain a pre-emulsion. The pre-emulsion was added to the reactor for 1.5 hours to

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perform a shell reaction, and then incubated for one hour. The reactor was maintained at 78°C and nitrogen washing was continued until the shell reaction was terminated. As a result, a latex acrylic impact modifier was obtained. The
5 latex acrylic impact modifier was subjected to coagulation with calcium chloride, dehydration, and drying, to give a powdery acrylic impact modifier.

(2) Preparation of mixture of impact modifier and
10 acrylic copolymer

90 g of the powdery acrylic impact modifier prepared in Section (1) and 10 g of the powdery acrylic copolymer prepared in Example 4 were mixed by a Henschel mixer with heating to 100°C to prepare a mixture of the impact
15 modifier and the acrylic copolymer.

(3) Preparation of vinyl chloride resin modified by
impact modifier and acrylic copolymer

100 g of a vinyl chloride resin (LS-100, LG Chemical
20 Co., Ltd.), 2.0 g of a tin-based thermal stabilizer, BT-107, 1.2 g of calcium stearate (Ca-St), 1.0 g of polyethylene wax (PE Wax), 1.5 g of a processing aid (PA822, LG Chemical Co., Ltd.), 14 g of a filler (CaCO₃), and 6 g of the mixture of the impact modifier and the acrylic copolymer

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prepared in Section (2) were mixed by a Henschel mixer with heating to 115°C to give a modified vinyl chloride resin.

(4) Measurement of extrusion output of vinyl chloride resin modified by impact modifier and acrylic copolymer

The vinyl chloride resin prepared in Section (3) was extruded by a twin screw extruder under processing temperature conditions of 170°C, 180°C, 185°C, and 190°C. A hot extrudate drawn away from a capillary die exit with diameter of 0.635 cm was cut into length of 0.8 cm to obtain extrudate pieces. The weights of three collections of the extrudate pieces were measured and averaged (?). The result is presented in Table 3 below.

(5) Charpy impact strength test of vinyl chloride resin modified by impact modifier and acrylic copolymer

The vinyl chloride resin prepared in Section (3) was milled by 2-roll mill at 190°C for 7 minutes to obtain 0.6mm sheets. The sheets were cut into size of 150mm×200mm and laminated in a predetermined milling direction on molds of 3mm×170mm×220mm. The resultant laminates were preheated by a 195°C heating press for 8 minutes (0.5 kg), pressed for 2 minutes (10 kg), and cooled for 3 minutes (10 kg) to obtain 3 mm-thickness

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specimens. The impact strength of the specimens was measured at 23°C and -10°C according to ASTM D-256 standard and the result is presented in Table 3 below.

5 (6) Measurement of melt time of vinyl chloride resin
modified by impact modifier and acrylic copolymer

The melt time of the vinyl chloride resin of Section (3) was measured in the same manner as in Example 11 and the result is presented in Table 3 below.

10

[Example 22]

A vinyl chloride resin was prepared in the same manner as in Example 21 except that 85 g of the powdery acrylic impact modifier prepared in Section (1) of Example
15 21 and 15 g of the powdery acrylic copolymer prepared in Example 4 were used. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3 below.

20 [Example 23]

A vinyl chloride resin was prepared in the same manner as in Example 21 except that 80 g of the powdery acrylic impact modifier prepared in Section (1) of Example 21 and 20 g of the powdery acrylic copolymer prepared in

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Example 4 were used. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3 below.

5 [Example 24]

A vinyl chloride resin was prepared in the same manner as in Example 21 except that 208.40 g of the latex acrylic impact modifier prepared in Section (1) of Example 21 and 23.61 g of the latex acrylic copolymer prepared in
10 Example 4 were mixed followed by coagulation with calcium chloride, dehydration, and drying. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3 below.

15

[Example 25]

A vinyl chloride resin was prepared in the same manner as in Example 21 except that 196.82 g of the latex acrylic impact modifier prepared in Section (1) of Example
20 21 and 35.41 g of the latex acrylic copolymer prepared in Example 4 were mixed followed by coagulation with calcium chloride, dehydration, and drying. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3

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below.

[Example 26]

A vinyl chloride resin was prepared in the same
5 manner as in Example 21 except that 185.25 g of the latex
acrylic impact modifier prepared in Section (1) of Example
21 and 47.22 g of the latex acrylic copolymer prepared in
Example 4 were mixed followed by coagulation with calcium
chloride, dehydration, and drying. The extrusion output,
10 impact strength, and melt time of the vinyl chloride resin
were measured and the results are presented in Table 3
below.

[Comparative Example 15]

15 A vinyl chloride resin was prepared in the same
manner as in Example 21 except that 95 g of the powdery
acrylic impact modifier prepared in Section (1) of Example
21 and 5 g of the powdery acrylic copolymer prepared in
Example 4 were used. The extrusion output, impact strength,
20 and melt time of the modified vinyl chloride resin were
measured and the results are presented in Table 3 below.

[Comparative Example 16]

A vinyl chloride resin was prepared in the same

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manner as in Example 21 except that 70 g of the powdery acrylic impact modifier prepared in Section (1) of Example 21 and 30 g of the powdery acrylic copolymer prepared in Example 4 were used. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3 below.

[Comparative Example 17]

A vinyl chloride resin was prepared in the same manner as in Example 21 except that 100 g of the powdery acrylic impact modifier prepared in Section (1) of Example 21 was used in the absence of the acrylic copolymer prepared in Example 4. The extrusion output, impact strength, and melt time of the vinyl chloride resin were measured and the results are presented in Table 3 below.

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Table 3

Section		Phase of acrylic copolymer and impact modifier mixture	Acrylic copolymer (wt%)	Impact modifier (wt%)	Extrusion output (g)	Impact strength (kgcm/cm)		Melt time (sec.)
						23℃	-10℃	
Example	21	Powder	10	90	1.07	26.8	8.1	102
	22	Powder	15	85	1.09	27.5	8.3	94
	23	Powder	20	80	1.15	29.1	8.6	90
	24	Latex	10	90	1.05	27.1	8.2	105
	25	Latex	15	85	1.07	28.3	8.5	89
	26	Latex	20	80	1.12	28.9	8.7	90
Comparative Example	15	Powder	5	95	1.02	22.4	6.9	110
	16	Powder	30	70	1.17	21.9	7.1	76
	17	Powder	-	100	0.95	22.4	7.6	121

As shown in Table 3, the vinyl chloride resins of

5 Examples 21-26 prepared using a mixture comprising 5-30 wt% of an acrylic copolymer prepared according to the present invention and 70-95 wt% of an impact modifier exhibited excellent impact strength and processability, regardless of whether the impact modifier and the acrylic copolymer were

10 mixed in a powder or latex phase. Here, the processability was evaluated by the extrusion output and the melt time. As the extrusion output increases, the processability increases. The melt time may vary according to used conditions. However, in view of foaming conditions, the

15 melt time is preferably in a range of 80-110 seconds, and

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optimally 90 seconds. In this regard, the vinyl chloride resin of Comparative Example 15, in which 95 parts by weight of the impact modifier and 5 parts by weight of the acrylic copolymer were used, did not sufficiently exhibit
5 the processability of the acrylic copolymer, thereby lowering the processability of the vinyl chloride resin. The vinyl chloride resin of Comparative Example 16, in which 70 parts by weight of the impact modifier and 30 parts by weight of the acrylic copolymer were used,
10 exhibited a low impact strength due to a counteractive effect of the acrylic copolymer on the impact modifier. The vinyl chloride resin of Comparative Example 17, in which only the impact modifier was used, exhibited very long melt time and poor processability that induces a non-
15 uniform formed product, and low impact strength.

Industrial Applicability

As apparent from the above description, when an acrylic copolymer prepared by the method of the present
20 invention is added to a vinyl chloride resin composition in a predetermined amount, the processability of the vinyl chloride resin can be enhanced, resulting in an excellent foamed product. Combination of the acrylic copolymer with an impact modifier can further enhance the impact strength

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of the vinyl chloride resin.

While the present invention has been particularly shown and described with reference to exemplary embodiments thereof, it will be understood by those of ordinary skill
5 in the art that various changes in form and details may be made therein without departing from the spirit and scope of the present invention as defined by the following claims.